

**R E M A R K S**

Entry of the above amendments is earnestly solicited. An early and favorable first action on the merits is earnestly solicited.

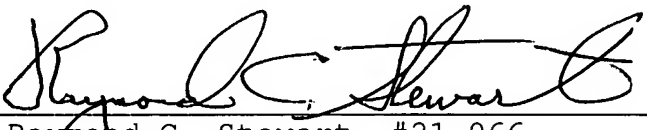
**Attached hereto is a marked-up version of the changes made to the application by this Amendment.**


Should there be any outstanding matters that need to be resolved in the present application, the Examiner is respectfully requested to contact Rick Gallagher (Reg. 28,781) at the telephone number of the undersigned below.

If necessary, the Commissioner is hereby authorized in this, concurrent, and future replies, to charge payment or credit any overpayment to Deposit Account No. 02-2448 for any additional fees required under 37 C.F.R. § 1.16 or under 37 C.F.R. § 1.17; particularly, extension of time fees.

Respectfully submitted,

BIRCH, STEWART, KOLASCH & BIRCH, LLP

By   
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RCS/RG:bmp  
0152-0586P  
Attachments

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(Rev. 12/19/01)

**VERSION WITH MARKINGS TO SHOW CHANGES MADE**

In the Specification:

The paragraph beginning on page 5, line 27 to page 6, line 5, has been amended as follows:

--5. An article of manufacture selected from the group consisting of mechanical working components, [outsect] outsert chassis resin components, chassis structures, trays and side plates obtained by molding, cutting, or molding and cutting the polyoxymethylene resin composition according to any one of the above-mentioned items 1 to 3. --

The paragraph beginning on page 7, line 28 to page 8, line 4, has been amended as follows:

--Various selections of these polymers can be used, depending on desired purposes. From the viewpoint of slidability or rigidity, oxymethylene homopolymers or oxymethylene copolymers having a low [component] comonomer content are preferable, whereas from the viewpoint of the heat stability or impact resistance, oxymethylene copolymers having a high comonomer content or block copolymers of hydrogenated polybutadiene and an oxymethylene copolymer are preferable. --

The paragraph beginning on page 8, line 17 to line 19, has been amended as follows:

--Use of an antioxidant and/or a [formalidehyde]  
formaldehyde - or formic acid-trapping agent or simultaneous use thereof is effective for heat stabilization. --

The paragraph on page 10, line 19 to line 26, has been amended as follows:

--A process for producing such polyether ester amides is disclosed in the above-mentioned JP-A-59-191752, U.S. Patent No. 5652326, etc. Polyether ester amides can be also produced by processes disclosed in detail in U.S. Patent No. 4230838, U.S. Patent No. 4332920, [U.S. Patent No. 4207410], U.S. Patent No. 4207410, U.S. Patent No. 4345064, U.S. Patent No. 4429081, etc.--

The paragraph beginning on page 10, line 27 to page 11, line 8, has been amended as follows:

-- Polyether amides can be produced by polycondensation of (1) polyamide-formable monomer and (2) polyethers having amino terminals and/or carboxyl terminals and (3) by copolycondensation of the terminals of (2) with a substantially

equivalent weight of aliphatic, [alicyclic] alicyclic, and aromatic dicarboxylic acids and/or diamines. Such polyether amides can be produced by process disclosed in the above-mentioned JP-A-4-168145, etc., which document is hereby expressly incorporated herein by reference. --

The paragraph beginning on page 12, line 13 to line 23, has been amended as follows:

-- Monomers copolymerizable with said  $\alpha$ -olefins include, for example, conjugated diene components (butadiene, isoprene, piperylene, etc.), non-conjugated dienes (1,4-hexadiene, cyclopentadiene, 5-[ethylidenenorbonene] ethylidenenorbornene, 2,5-norbonadiene, etc.), (meth)acrylic acid or its ester derivatives (methyl methacrylate, etc.), (meth)acrylonitrile, aromatic vinyl monomers (styrene,  $\alpha$ -methylstyrene, vinyltoluene, p-t-butylstyrene, etc.), vinyl ethers (vinylmethylether, etc.), vinyl esters (vinyl acetate, etc.). --

The paragraph beginning on page 18, line 20 to page 19, line 5, has been amended as follows:

--It is preferable from the viewpoint of imparting desirable surface appearance and slidability to molded articles to use inorganic fillers having particle sizes of not more than

100  $\mu\text{m}$  in terms of volume average particle size, more preferably not more than 50  $\mu\text{m}$ , most preferably not more than 30  $\mu\text{m}$ .

Inorganic fillers for use for the purpose are preferably potassium titanate whiskers, wollastonite (acicular and granular), calcium carbonate, talc, graphite, nepheline, syenite, hydroxyapatite, silica, carbon black, and kaolin.

Particularly preferable are potassium titanate whiskers, wollastonite (acicular and granular), calcium carbonate, talc and carbon black. --

The paragraph beginning on page 26, line 19 to page 27, line 7, has been amended as follows:

-- b-2: 500 parts by weight of caprolactam, 450 parts by weight of polyethylene glycol, 66 parts by weight of adipic acid and 5 parts by weight of antioxidant (Irganox 1098, made by Ciba Specialty chemicals Co., Ltd.) were charged into a 3-liter stainless steel [autoclave] autoclave, followed by heating at 260°C for one hour with stirring in a nitrogen atmosphere to obtain a homogeneous transparent solution. Then, 1.0 parts by weight of an antimony trioxide catalyst was added thereto. Then, the pressure was reduced to 1 mmHg or less over one hour, and then reaction was carried out for 3 hours. The resulting viscous polymer was placed in a strand shape onto a belt and

pelletized to obtain polyether ester amide. The polyether ester amide so obtained had a relative viscosity of 2.0 (0.5 wt.%, m-cresol solution, 25°C) and had the following copolymer composition based on NMR determination; --

The paragraph beginning on page 28, line 18 to line 21, has been amended as follows:

--c-3: Maleic acid-modified straight chain, low density polyethylene having a maleic acid modification [rte] rate of 1.5 wt.% and a melt index of 3.0 g/10 min. (ASTM D-1238-57T); --

The paragraph beginning on page 28, line 26 to page 29, line 3, has been amended as follows:

-- c-5: Maleic acid-modified, hydrogenated styrene-butadiene block copolymer having a maleic acid modification rate of 1.0 wt.% and a melt index of 0.4 g/10 min. (ASTM D-1238-57T), obtained by modifying Tuftec H 1052 of [styrone] styrene/butadiene=20/80 wt.% (made by Asahi Kasei Co.) with maleic anhydride; --

The paragraph beginning on page 30, line 5 to line 7, has been amended as follows:

--e-1: {Ganular] Granular wollastonite having a volume average particle size of 3  $\mu\text{m}$ , measured by a laser particle size meter and an aspect ratio of 3; --

In Table 3 on page 39, in the third column from the right, the text has been amended to read Decomposition and foaming during extrusion

The paragraph beginning on page 46, line 1 to line 14, has been amended as follows:

--Example 26

96 parts by weight of polyoxymethylene resin (a-5) containing 0.3 wt.% of triethylene glycol-bis-[3-(3-t-butyl-5-methyl-4-hydroxyphenyl)propionate], 0.05 wt.% of polyamide 66 and 0.10 wt.% of calcium stearate as stabilizers, 2 parts by weight of polyamide elastomer (b-1) and 2 parts by weight of acid-modified olefinic resin (c-1) [bioxial] biaxial extruder, 30 mm in diameter (L/D=30), set to 200°C at a screw revolution rate of 200 rpm and a feed rate of 10 kg/hr. The extruded resin was pelletized by a strand cutter, and subjected to evaluation

of the above-mentioned properties. Results are shown in Table 7. --

The paragraph beginning on page 50, line 5 to line 23, has been amended as follows:

--Example 32

95 parts by weight of polyoxymethylene resin (a-5) containing 0.3 wt.% of triethylene glycol-bis-[3-(3-t-butyl-5-methyl-4-hydroxyphenyl)propionate] and 0.05 wt.% of polyamide 66 as stabilizers, 2.5 parts by weight of polyamide elastomer (b-1), 2.5 parts by weight of acid-modified olefinic resin (c-1), 7 parts by weight of electroconductive carbon black (e-2), and one part by weight of triphenylphosphine, 2 parts by weight of epoxy resin (ARALDITE ECN 1299 made by Asahi Kasei Epoxy K.K.) and 0.3 parts by weight of [dicyaniamide] dicyandiamide as stabilizers were uniformly blended in a blender and melt kneaded by a biaxial extruder, 30 mm in diameter (L/D=30), set to 200°C at a screw revolution rate of 200 ppm and a feed rate of 10 kg/hr. The extruded resin was pelletized by a strand cutter. The pellets so obtained were subjected to evaluation of the above-mentioned properties. Results are shown in Table 8. --